

# Design of micro radial turboexpanders for ORC power cycles: from 0D to 3D

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## Abstract

The 3D design and analysis of a 5 kW micro turbo expanders for small, distributed ORC power units is proposed, starting from a recently developed 0D design tool, which was initially applied to 50 kW radial turbines.

The turbine was sized referring to R134a as working fluid. At the same time, the main performance parameters, kinematic conditions and the different loss sources were determined. The resulting 0D basic geometry and the related non-dimensional parameters were used as the starting point to define the 3D geometry of the rotor (distribution of the metal blade angles and of the thickness profile) and to refine some design parameters like the number of blades.

On the basis of the 3D blade profile and flow channels, a computational grid was generated. The CFD analysis of the rotor was carried out by means of Ansys Fluent® software, including a real-gas Equation Of State (EOS) model for the working fluid.

28 The design of the rotor was reconsidered as a consequence of the 3D CFD approach. Finally, the comparison  
29 between the 0D and 3D results was carried out, showing a good agreement between the two approaches and,  
30 thus, verifying the reliability of the combined 0D – 3D design tool for micro-size turboexpanders of ORCs.

31

## 32 **Keywords**

33 ORC Expander, Micro Radial Inflow Turbine, 0D – 3D Turbine Design, Blade loading , Turbine losses

34

## 35 **1. Introduction**

36 Research, development and commercialization of Organic Rankine Cycles (ORC) have been in strong growth  
37 over the last years, in consequence of the increasing demand of energy recovery from low-value resources (like,  
38 for example, low temperature heat sources in the 90 – 200 °C range). The ORC technology is suitable and reliable  
39 for mini and micro Combined Heat and Power applications (CHP), with special reference to low size (from a few  
40 tens to some hundreds kW). ORCs have a wide range of potential applications as low grade heat recuperators,  
41 such as industrial heat waste, renewables and even domestic applications like internal combustion engines [1, 2],  
42 solar and geothermal resources [3 – 8]. However, micro-scale ORC based CHP units (< 10 kWel), having a great  
43 potential to meet buildings energy demand, have not yet demonstrated their applicability at experimental and  
44 commercial level [9].

45 Only a few studies are found in the technical literature about this small power size, many of which are  
46 focused in the selection of the working fluids and in assessing the most suitable expander technologies [10]. Most  
47 researchers focus on scroll expanders, which are usually adapted from compressors for refrigeration equipment.  
48 This solution is certainly interesting: however, its potential is limited, both in terms of achievable efficiency  
49 (usually less than 60%), and of other unfavorable issues such as leakages and, due to the large wetted surface,  
50 friction and heat transfer losses [11]. Similar negative issues affect other types of volumetric expanders like the  
51 screw ones. In this field of technology, systems for cost effective power production at outputs within the range of  
52 20 – 50 kWel were developed, whereas micro – scale screw expanders (< 10 kWel) are difficult to achieve in the  
53 current market. For example, Ormat and ElectraTherm commercialize ORC equipped with these expanders in the  
54 range of 50+ kWel [10].

55 The development of a micro-scale dynamic expander represents a major challenge. Dynamic expanders have  
56 proven to be reliable and able to achieve high efficiencies in larger sizes (typically, higher than 50 – 100 kWel [10]):  
57 in order to extend their field of application to micro-scale for distributed energy conversion systems, a

58 preliminary screening is certainly needed, assessing issues such as rotational speed, sizing and manufacturing.  
59 These are among the main reasons behind the present work.

60 Literature lacks of modelling and/or experimental studies to assess the design feature and operating issues of  
61 micro turbo expanders within kW scale, which is a field typically covered by volumetric machines like scrolls,  
62 screw and reciprocating units [10]. Recently, Rahbar et al. [12] proposed a methodology for the preliminary and  
63 refined design of radial turbines for low power capacity, coupling mean-line modelling and CFD analysis. Anyhow,  
64 their calculations were referred to air as working fluid. Successively, Rahbar et al. [13] presented a novel approach  
65 for modelling and optimization of ORC based on a small-scale radial turbine. It merges the ORC cycle with the  
66 mean-line modelling of radial inflow turbine combined with integrated optimization technique, but is applied to a  
67 40 – 100 kW size range.

68 In the following, a design procedure for micro radial ORC turbines (kW class size) is introduced, starting from  
69 a 0D tool for the basic sizing (initially applied to a 50 kW turbine) and then using a 3D approach to refine the  
70 design by (i) improving the blade geometry and (ii) redefining the most accurate number of blades, in order to  
71 achieve a proper blade loading and a good flow guidance thus maximizing the performance of the impeller.  
72 Moreover, the CFD calculation of the rotor is useful to validate the actual downscale potential of the developed  
73 OD code, and the limits in the scalability of the different types of losses. The results of the basic OD and the  
74 refined 3D design procedures were compared to validate the ability of the OD model to provide a reliable  
75 preliminary design of the rotor.

76

## 77 **2. Preliminary design with OD model**

78 The first step of the design process is carried out using a 0-D model [14, 15], which guides the user to  
79 perform a preliminary sizing of the radial expander evaluating its performance, considering several possible ORC  
80 working fluids and rotor geometries (i.e. radial and backswept blades). Reference [14] contains the fundamental  
81 guidelines for the correct choice of the main non-dimensional design parameters, such as the *Work coefficient*  
82 ( $\Psi$ ), *Flow coefficient* ( $\Phi$ ), and *Degree of reaction* ( $R$ ); a second set of non-dimensional geometrical parameters,  
83 derived from the fundamental reference literature [16, 17, 18], helps to produce a reasonable design of the  
84 machine. In order to facilitate the reader, the main steps are here shortly summarized.

85 The preliminary sizing and calculation of the turbine geometry is started using the basic input data (rated  
86 power output, thermodynamic in/out conditions) and a set of non-dimensional parameters chosen by the  
87 designer within a reasonable range, on the basis of the fundamental literature references, having in mind the  
88 achievement of a small rotor diameter and a reasonable rotational speed. The choice of the degree of reaction  
89 ( $R_s$ ) is driven on one hand to achieve the energy conversion in one single stage (thus high values would be

90 preferred), on the other hand to limit sealing problems even with open rotor design, relatively economic to  
91 manufacture with common machining or precision casting given the low size (low values of reaction degree are  
92 preferable in this view). At the same time, high values of the stage loading ( $\psi$ ) and of the flow coefficient ( $\phi$ ),  
93 compliant with maintaining the flow in a high subsonic or transonic regime, are selected whenever possible.

94 This first step allows to select the load and flow coefficients ( $\psi=\Delta h_0/u_2$  and  $\phi=c_{m2}/u_2$  respectively) and the  
95 isentropic degree of reaction  $R_s$ ; the acceptability of the fundamental parameters (Specific Diameter and Specific  
96 Speed) is also evaluated using the Balje Chart, that gives a reliable indication of the suitability of chosen design  
97 parameters. Referring to figure 1, it is further possible to define some non-dimensional geometrical parameters:  
98 the nozzle ratio  $D_1/D_2$ , the rotor ratio  $D_3/D_2$ , the diffuser ratio  $D_4/D_3$ , the Diffuser length – diameter ratio  $L_d/D_3$ ,  
99 the Rotor Aspect Ratio  $b_2/D_2$ , the Nozzle Height Ratio  $b_1/b_2$ . Then, the geometry of the vaned stator (IGV) is  
100 determined, as well as its number of blades.

101 A major issue in rotor design is the choice of the number of blades ( $Z_B$ ), which deeply affects the rotor  
102 geometry and the related losses. The existing literature applies correlations similar to Zweifel's load criterion [16,  
103 17] to calculate  $Z_B$ ; however, these were developed for large-size machines (often for completely different fluids  
104 and originally for axial-flow turbines), so that they become unreliable when applied to downscaled prototypes  
105 such as here proposed. The result is typically a high number of blades, and consequently an excessive solidity, and  
106 difficulties in manufacturing.

107 For this reason, it was decided to leave  $Z_B$  as a further input design variable, whose value should be chosen  
108 from a reasonable compromise between an effective guidance of the fluid through the vanes and a sufficiently  
109 low value of the losses between the wet surfaces. The idea was to adjust  $Z_B$  after an evaluation of the detailed  
110 CFD results. After  $Z_B$  is defined, the conditions for optimal incidence at rotor inlet can be defined applying proven  
111 correlations [16, 17].

112 The subsequent step of the OD design process is the evaluation of the expander losses and their effects on  
113 the efficiency of the expansion. Specifically, the relationships of losses with the non-dimensional design  
114 parameters ( $b_2/D_2$ ,  $\phi$ ,  $\psi$  and  $R_s$ ) are determined: the contributions include rotor incidence, skin friction, tip  
115 clearance, blade loading, disk friction and diffuser losses. The sensitivity of turbine losses and efficiency to  $\phi$ ,  $\psi$   
116 and  $R_s$  leads to a reasonably efficient preliminary OD design, which is the starting point for the 3D design  
117 refinement process.

118 With respect to the previous work of the Authors [14], the expander is downsized to 5 kW and the related  
119 implications in terms of losses and performance are assessed. The key dimensional variable of the 0-D design is  
120 the rotor *Inlet diameter* ( $d_2$ ), together with the thermodynamic data for *inlet total pressure* ( $p_{01}$ ) and *inlet total*

121 *temperature* ( $T_{01}$ ). The list of the dimensional and non-dimensional design parameters, referred to the sketch of  
122 figure 1, is shown on table 1.

123 The first-attempt choice was a rotor with 8 backswept blades, which was sized by the OD model, based on  
124 the data available on table 1 and using R134a as the working fluid. The main resulting design data are shown on  
125 table 2.

126 The results of the design exercise for the 5 kW turbine are compared in the following with those of the  
127 previous 50-kW class unit. The main issues are:

128 • the mass flowrate decreases from 1.749 kg/s (50 kW) to 0.1984 kg/s (5 kW), less than linearly due  
129 to the different degree of reaction, blade loading and flow coefficient. In particular, the downscaled  
130 version has a higher load coefficient ( $\psi$ ) and a lower flow coefficient ( $\phi$ ).

131 • The rotational speed is more than doubled, passing from 40,000 rpm to about 88,000 rpm,  
132 essentially because of the reduction of the rotor diameter (which is less than halved); this result agrees  
133 with the typical values of micro expanders reported in literature [13, 15].

134 • The overall loss coefficient is almost doubled, mainly due to the secondary flows resulting from  
135 the increased blade loading. The other sources of losses, like incidence, skin friction, tip clearance, disk  
136 friction and profile curvature, are less relevant, as can be seen in the pie-chart diagram of Figure 2  
137 showing the distribution of the rotor losses.

138 • The resulting total-to-static efficiency of the downsized 5 kW expander is about 8 % points lower  
139 (from 0.77 for the 50 kW turbine, to 0.69 for the 5 kW one). This value is in agreement with recently  
140 available literature data on radial micro-turbines [13, 15, 19, 20].

141

### 142 3. 3D design procedure: meshing and CFD

143 The verification of the design procedure by means of CFD was limited to the rotor, which is recognized as the  
144 critical component both for performance and technological challenge. The geometry resulting from the OD  
145 preliminary design was transferred into Ansys BladeGen® [21], including blade heights, radii and characteristic  
146 angles at the inlet/outlet sections. The geometry of the meridional channel was defined using typical shapes  
147 documented in the literature [16, 17] for radial turbines, which were non-dimensionalized and parametrized as a  
148 function of the Specific speed  $N_s$  (i.e. *Balje chart*). Furthermore, in order to define the internal geometry of the  
149 impeller, the distributions of the blade angles have to be defined; the blade angle ( $\beta$ ) and the wrap angle ( $\Theta$ ) are  
150 in the following relationship:

$$\tan \beta = \frac{d\theta}{dm} \quad (1)$$

151

152 where  $m$  is the meridional coordinate. As a first attempt, a linear distribution of  $\beta$  was considered; the choice  
153 of the  $\beta - m$  function, as well as the geometry of the meridional channel, allows the calculation of  $\Theta$  by the  
154 integration of Eq. (1).

155 Another relevant feature for the rotor design is the distribution of thickness along the camber line; here, a  
156 modified 4 digit series NACA profile (NACA 0005-55) was selected, symmetrical with reference to the mean line  
157 and having the maximum thickness located at 50% of the camber line. The resulting CAD 3D model of the impeller  
158 is shown in Figure 3.

159 In order to perform the CFD analysis of the turboexpander, the following step is the generation of a suitable  
160 computational grid. The discretization of the domain heavily affects the quality of the solution, both in terms of  
161 accuracy and computational costs. As a compromise between these two parameters, a mesh of 991,260  
162 hexahedral elements was created by means of Ansys Turbogrid® software [22]. The structured 3D mesh used in  
163 the simulations is shown in Figure 4 (representing the single blade passage which was used for the calculations).  
164 In the zone near to the blade surface and walls (hub and tip) the grid was refined; in order to maintain a good  
165 compromise between solution accuracy and computational costs, the first cell dimension  $y$  was defined assuming  
166 a target *Dimensionless Wall Distance*  $y^+$  of about 40 with a *Reynolds Number* of flow close to  $3e10^6$ . These choices  
167 are in accordance to the adopted  $k-\omega$  Turbulence model [23].

168 The software package Ansys Fluent® [23] was used to perform the computational analysis of the IFR turbine,  
169 selecting the model options described in the following.

170 *Numerical Model:* steady-state 3D viscous, single phase, compressible flow is used; due to the mesh  
171 elements type and topology, a first order upwind advection scheme was chosen because of its numerical stability,  
172 as suggested by [24]. Simulations were carried out using a RANS approach (Reynolds Averaged Navier Stokes  
173 equations), with the *standard*  $k-\omega$  turbulence model and the *Density-Based* solver. *Standard*  $k-\omega$  is an empirical  
174 model based on transport equations for the *turbulence kinetic energy* ( $k$ ) and the *specific dissipation rate* ( $\omega$ ). The  
175 transport equations implemented to achieve the *turbulent kinetic energy*  $k$  and the *specific dissipation rate*  $\omega$  are  
176 the following:

177

$$178 \quad \frac{\partial}{\partial t}(\rho k) + \frac{\partial}{\partial x_i}(\rho k u_i) = \frac{\partial}{\partial x_j} \left( \Gamma_k \frac{\partial k}{\partial x_j} \right) + G_k - Y_k + S_k \quad (2)$$

179

$$180 \quad \frac{\partial}{\partial t}(\rho \omega) + \frac{\partial}{\partial x_i}(\rho \omega u_i) = \frac{\partial}{\partial x_j} \left( \Gamma_\omega \frac{\partial \omega}{\partial x_j} \right) + G_\omega - Y_\omega + S_\omega \quad (3)$$

181

182 In order to accurately represent the behaviour and properties of the working fluid (R134a) assumed in the  
183 simulations, the cubic Soave-Redlich-Kwong (SRK) Equation of State was activated [25]. The coefficients are given

184 for each equation of state as a function of *critical temperature*  $T_c$ , *critical pressure*  $p_c$ , *acentric factor*  $a_f$ , and *critical*  
185 *specific volume*  $v_c$ . The physical properties of R134a are listed in Table 3.

186 *Boundary Conditions (BC):* first of all, the computational domain was suitably extended outside of blades area  
187 (figure 4), upstream of the *Leading Edge* (LE) and downstream of the *Trailing Edge* (TE), in order to avoid spurious  
188 reflections; the extension was about 10% and 50% of the chord length at inlet and outlet respectively. As the  
189 computation involved only the rotor, a Single Reference Frame (SRF) calculation was implemented, covering the  
190 entire domain; the rotational speed was set at the value provided by the preliminary OD design. The mass flow  
191 rate, total temperature and inlet velocity components calculated by the OD model were assumed as known inputs  
192 of the 3D model at the rotor inlet; their uniform local values at the upstream inlet of the domain were  
193 determined by applying the mass, momentum and Rothalpy conservation equations. The setup of the mass flow  
194 rate inlet boundary condition required some attention; in fact, the OD model design gives the flow parameters  
195 corresponding to the blade leading edge, whereas the CFD domain is extended upstream. In the definition of  
196 boundary conditions, this effect must be taken into account and the flow direction must be assigned in order to  
197 obtain the correct value at the leading edge. In practice, there is an extended region of unguided, rotating  
198 channel upstream of the actual expander inlet. Within this region, a considerable variation of the velocity  
199 components takes place, which is relevant in this case (and generally for this kind of turboexpanders),  
200 characterized by a considerable variation of the radial coordinate from the upstream inlet to LE section and by a  
201 high rotational speed of the impeller (a consequence of the very small size). The calculation of the flow direction  
202 is done applying the mass balance, free vortex and Conservation of Rothalpy equations, respectively:

203

$$204 \quad \rho_2 r_2 w_{m2} = \rho_i r_i w_{mi} \quad (4)$$

$$205 \quad r_2 c_{u2} = r_i c_{ui} = \text{constant} \quad (5)$$

$$206 \quad h_2 + \frac{1}{2} w_2^2 - \frac{1}{2} u_2^2 = h_i + \frac{1}{2} w_i^2 - \frac{1}{2} u_i^2 \quad (6)$$

207 where the subscript  $i$  represents the upstream inlet section.

208 The applied boundary conditions for the simulations are:

- 209 - Mass Flow ( $\dot{m}$ ), Flow direction and Total Temperature ( $T_{02}$ ) at the inlet;
- 210 - Static Pressure ( $p_3$ ) at the outlet;
- 211 - Rotational Periodicity at the lateral interfaces;
- 212 - Rotational, adiabatic wall for the blade and hub surface

213

#### 214 **4. Results of the *first-attempt* 3D design**

215 The purpose of the simulations for the "first attempt" geometry, was the qualitative evaluation of the  
216 impeller flow conditions in order to develop a modified impeller geometry with improved performance. Already in  
217 this phase of the procedure, a comparison between the two design approaches (OD and 3D CFD) can be  
218 performed in order to assess the issues and reliability of the OD model and providing, at the same time, a gross  
219 check of the 3D calculations. Table 4 reports the main results achieved by the numerical 3D simulations, whereas  
220 table 5 shows the comparison between OD and 3D CFD design for the first attempt geometry.

221 The power output  $P$  was calculated by the total enthalpy drop across the rotor (3), using the mass-weighted  
222 average values of enthalpy obtained from the CFD analysis, evaluated at the LE and TE sections.

$$P = \dot{m}(h_{02} - h_{03}) \quad (7)$$

223 The isentropic Total-to-Static efficiency of the rotor was calculated as:

$$\eta_{ts} = \frac{h_{02} - h_{03}}{h_{02} - h_{3is}} \quad (8)$$

224 Which represents the ratio between the actual and the maximum theoretical specific work of the expander  
225 for the given in/out conditions. Here again, the mass-averaged values were applied. As the study involves a single-  
226 stage machine without diffuser, the total-to-static efficiency includes the contribution of the kinetic energy lost at  
227 the rotor outlet.

228 From the analysis of the results, the following issues were determined:

229 1) The power output calculated with the first-attempt 3D procedure (4,504 W ) is about 10% lower than that  
230 resulting from the OD design( 5,093 W). This is due to the non-optimal guidance of the fluid by the blade, which  
231 leads to a positive average mass-averaged value of the angle of deviation at rotor output (thus resulting in a  
232 power loss based on Euler's equation [16]). The relevant error on  $c_3$  is also due to the difference in the tangential  
233 component.

234 2) The shape of the meridional channel induces a heavy reduction of the velocity (diffusion) in the middle of  
235 the channel zone, close to the hub surface (figure 5).

236 3) Observing the Blade Loading diagram comparison in the blue lines of Figure 5 (first-attempt geometry;  
237 Figure 5 shows the pressure profiles on the SS and PS along the non-dimensional meridional coordinate), the hub  
238 region is clearly lightly loaded, with small differences between Pressure Side and Suction Side pressure



239 distributions. Moreover, along the entire blade height, it is highlighted an unsatisfactory overlapping of the  
240 pressure distributions in the LE zone.

241

## 242 **5. Results of the *improved* 3D design**

243 In order to improve the above unsatisfactory aspects related to the first attempt 3D design of the rotor,  
244 mainly attributable to the fluid behaviour through the machine, some modifications to the impeller geometry  
245 were considered. The first-attempt design showed a non-optimal guidance of fluid. This significantly affects the  
246 power output (7), because it determines a relatively large tangential component of absolute velocity at the TE  
247 ( $c_{u3}$ ). For this reason, the number of blades was increased from 8 to 10. Another relevant aspect is the shape of  
248 the meridional channel; the first attempt geometry produced an unsatisfactory expansion of the fluid, especially  
249 in the near-hub zone where some recirculation and very low velocities were noticed. Therefore, the shape of the  
250 meridional channel and the distribution of  $\beta$  and  $\theta$  angles were modified (Figure 6). Figure 7 shows the improved  
251 geometry of the impeller.

252 Observing the blade loading for the improved geometry (red lines in figure 5) it is clear that a large fraction of  
253 load is re-located at the central part of the profile, on each of the considered layers (10%, 50% and 90% span). In  
254 addition, the rapid increase of velocity on the Suction Side (shown in Figure 5, 50% span) implies that the largest  
255 fraction of pressure drop is already achieved at about 40% of the camber line; this effect is emphasized  
256 approaching the shroud region. As it can be seen, with respect to the first-attempt Blade Loading curves (blue  
257 lines), a better work extraction in the near-hub zone is achieved. Furthermore the load has a more homogeneous  
258 distribution along the blade's height, which is important in order to limit secondary flow effects.

259 The contours of relative velocity at 50% blade height are reported in Figure 8. A local recirculation along the  
260 first 20% of the pressure side is noticeable; while in the first part of the suction side, high values of relative  
261 velocity were registered, which are due to the high profile curvature in this zone. The maximum relative Mach  
262 number inside the vane is about 0.54.

263 A qualitative assessment of the improvement of the rotor design can be done comparing the Relative Mach  
264 ( $M_{rel}$ ) distributions on meridional surface (Figure 9).

265 After the modification of the geometry it is possible to register a more satisfactory behaviour of the flow  
266 through the meridional channel, with a smoother expansion of the fluid from the inlet to the outlet and a removal  
267 of the aforementioned diffusion bubble in the near-hub zone. The main results of the modified geometry are  
268 summarized in table 6.

269

## 270                   **6. Comparison between 0D and 3D: Results and discussion**

271           The last part of this work deals with the comparison between the overall results of the zero-dimensional  
272 design and those of the three-dimensional CFD (these last are obtained by mass-averaging the results of the flow  
273 computation on the inlet and outlet sections), both for the improved geometry. Table 7 shows the comparison  
274 between the most relevant parameters calculated with the 0D and 3D CFD models, both related to the improved  
275 geometry.

276           On the whole, the significant calculated parameters are in fair agreement for the two approaches. It is  
277 interesting to compare the absolute velocities calculated at the leading and trailing edge sections. A lower  
278 agreement was found for the magnitude of the absolute velocity  $c_3$ , which is slightly higher in the 3D design. The  
279 isentropic total-to-static efficiency shows a very satisfactory agreement, with a 0D – 3D relative error within 1,5%.  
280 Finally, the two models predict close values of power output, with a relative error less than 5%.

281

## 282                   **7. Conclusions**

283           Starting from a previously developed 0D design tool for radial ORC expanders [14], specifically tuned on a 50  
284 kW machine and able to account for the specific loss correlations across the rotor, a 3D design procedure for very  
285 small expanders (power rating 5 kW) was developed with the purpose of achieving an improved design, mainly  
286 concerning the geometry of the flow channel and the number of blades.

287           The results of the 0D tool (requiring reduced computational time, thus very suitable to be used as a  
288 preliminary design) are the basis for the definition of the geometry of the expander. Compared to many existing  
289 literature 3D models, the here developed one considered the real behaviour of the working fluid, by means of SRK  
290 EOS.

291           The 3D geometry of the rotor was imported in commercial CFD packages [21-24]. The 3D approach is applied  
292 at two different levels, first-attempt (the geometry is a simple outcome of the 0D design) and improved (the  
293 geometry is revised after a computer-assisted evaluation of the shortcomings of the first-attempt). The improved  
294 design corresponds to the final fluid dynamics design of the rotor, with the improved blade geometry and a more  
295 suitable number of blades (which is not directly provided by the traditional 0D correlations), determining a  
296 correct blade loading which is not achievable applying 0D design guidelines.

297           The results of the 0D and 3D models applied to the reference case (a 5 kW machine operating with R134a)  
298 showed a satisfactory agreement, confirming the reliability of the 0D design tool as the basis for the definition of  
299 the overall geometry and working parameters of the machine. The coupling of the two approaches appears to  
300 represent a reliable design procedure for small and micro radial turbines working with organic fluids in ORCs.

301	<b>Nomenclature</b>	
302	$a_f$	Acentric factor
303	$b$	blade height [m]
304	$c$	absolute velocity [m/s]
305	$d$	diameter [m]
306	$h$	enthalpy [J/kg]
307	$k$	Turbulence kinetic energy [J/kg]; Thermal Conductivity [W/m-K]
308	$Ma$	Mach number
309	$\dot{m}$	mass flow rate [kg/s]
310	$M_w$	Molecular Weight [kg/kmol]
311	$N_s$	specific rotational speed [rpm]
312	$p$	pressure [Pa]
313	$P$	power output [kW]
314	$r$	radius [m]
315	$R$	Degree of reaction
316	$T$	temperature [K]
317	$u$	peripheral velocity [m/s]
318	$V_{sound}$	sound speed [m/s]
319	$v$	Specific volume [m <sup>3</sup> /kg]
320	$w$	relative velocity [m/s]
321	$Z$	number of blades of the rotor
322		
323	<u>Greeks</u>	
324	$\alpha$	Absolute flow angle (from radial direction, positive in the u direction) [°]

325	$\beta$	Blade Angle; Relative flow angle (from radial direction, positive in the u direction) [°]
326	$\Delta$	Variation
327	$\xi$	Loss coefficient
328	$\eta$	Efficiency
329	$\Theta$	Blade Wrap angle [°]
330	$\mu$	Dynamic viscosity [Kg/s-m]
331	$\nu$	Kinematic viscosity [m <sup>2</sup> /s]
332	$\rho$	Density [kg/m <sup>3</sup> ]
333	$\Phi$	Flow coefficient
334	$\Psi$	Load coefficient
335	$\omega$	Specific dissipation rate
336	$\Omega$	Angular velocity [rpm]

337

338 Subscripts/Superscripts

339	0	total value (stagnation)
340	1, 2, 3, 4	referred to sections 1, 2, 3, 4 (figure 1)
341	c	critical
342	D	diffuser
343	is	isentropic
344	m	meridional component
345	ts	total to static
346	u	peripheral
347	—	mass-average

348

349 Acronyms

350	CFD	Computational Fluid Dynamics
351	IFR	Inflow Radial (turbine)
352	NACA	National Advisory Committee for Aeronautics
353	ORC	Organic Rankine Cycle

354

355 **References**

356 [1] Vaja, I., Gambarotta, A., 2010, "Internal Combustion Engine (ICE) bottoming with Organic Rankine  
357 Cycles (ORCs)", *Energy*, 35 , 1084–1093.

358 [2] Schuster, A., Karellas, S., Kakaras, E., Spliethoff, H., 2009, "Energetic and economic investigation of  
359 Organic Rankine Cycle applications", *Applied Thermal Engineering*, 29, 1809–1817.

360 [3] Zhai, H., Dai, Y.J., Wu, J.Y., Wang, R.Z. , 2009, "Energy and exergy analyses on a novel hybrid solar  
361 heating, cooling and power generation system for remote areas", *Applied Energy*, 86 , 1395–1404.

362 [4] Fiaschi, D., Lifshitz, A., Manfrida, G., Tempesti, D., 2014, "An innovative ORC power plant layout for  
363 heat and power generation from medium- to low-temperature geothermal resources", *Energy Conversion and  
364 Management*, 88, 883-893.

365 [5] Di Pippo, R., 2006, "Geothermal Power Plants: Principles, Applications and Case Studies", *Elsevier  
366 Advanced Technology*, London, UK.

367 [6] Heberle, F., Brüggemann, D., 2006, "Exergy based fluid selection for a geothermal Organic Rankine  
368 Cycle for combined heat and power generation", *Applied Thermal Engineering*, 30, 1326-1332.

369 [7] Lentz, A., Almanza, R., 2006, "Solar–geothermal hybrid system", *Applied Thermal Engineering*, 26,  
370 1537–1544.

371 [8] Dai, Y., Wang, J., Gao, L., 2009, "Parametric optimization and comparative study of organic Rankine  
372 cycle (ORC) for low grade waste heat recovery", *Energy Conversion and Management*, 50, 3, 576-582.

373 [9] Dong, L.L., Liu, H., Riffat, S.B., 2009, "Development of small-scale and micro-scale biomass-fuelled CHP  
374 systems" - A literature review, *Applied Thermal Engineering*, 29, 2119-2126.

- 375 [10] Qiu, G., Liu, H., Riffat, S., 2011, "Expanders for micro-CHP systems with organic Rankine cycle",  
376 *Applied Thermal Engineering*, 31, 16, 3301-3307.
- 377 [11] Song, P., Wei, M., Shi, L., Syed Noman Danish, Chaochen Ma, 2015 "A review of scroll expanders for  
378 organic Rankine cycle systems", *Applied Thermal Engineering*, 75, 22, 54-64.
- 379 [12] Rahbar, K., Mahmoud, S., Al-Dadah, R.K., 2014, "Mean-line modeling and CFD analysis of a miniature  
380 radial turbine for distributed power generation systems", *International Journal of Low-Carbon Technologies*, 0,  
381 1-12.
- 382 [13] Rahbar, K., Mahmoud, S., Al-Dadah, R.K., Moazami, N., 2015, "Modelling and optimization of organic  
383 Rankine cycle based on a small-scale radial inflow turbine", *Energy Conversion and Management*, 91, 186-198.
- 384 [14] Fiaschi, D., Manfrida, G., Maraschiello, F., 2015 "Design and performance prediction of radial ORC  
385 turboexpanders", *Applied Energy*, 138, 517-532.
- 386 [15] Micheli, D., Reini, M., 2007, "On bottoming a micro turbine with a micro ORC section: Part a)  
387 preliminary design of the ORC expander", *Proceedings of ECOS Conference, Padova*, 1025-1033.
- 388 [16] Dixon, S.L., 1998, "Fluid Mechanics and Thermodynamics of Turbomachinery", Fifth Edition, *Elsevier*  
389 *Butterworth-Heinemann*.
- 390 [17] Whitfield, A., Baines, N.C., 1990, "Design of Radial Turbomachines", *Longman Scientific and Technical*.
- 391 [18] Rohlik, H. E., 1975, "Radial Inflow Turbines," NASA SP 290, Vol. 3, Ch. 10.
- 392 [19] Matsuura, K., Kato, C., Yoshiki, H., Matsuo, E., 2003, "Prototyping of Small-sized Two-dimensional  
393 Radial Turbines", *IGTC Tokyo*, 1-7.
- 394 [20] Aghaali, H., Hajilouy-Benisi, A., 2008, "Experimental modeling of twin-entry Radial Turbine", *Iranian*  
395 *Journal of Science and Technology*, 32, 571-584.
- 396 [21] ANSYS Inc., 2011, "ANSYS TurboSystem User's Guide".
- 397 [22] ANSYS Inc., 2011, "ANSYS TurboGrid User's Guide".
- 398 [23] ANSYS Inc., 2011, "ANSYS FLUENT Theory Guide".
- 399 [24] ANSYS Inc., 2011, "ANSYS FLUENT User's Guide".

400 [25] Soave, G., 1972, "Equilibrium constants from a modified Redlich–Kwong equation of state", *Chemical*  
401 *Engineering Science*, 27, 1197-1203.

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## Figures captions

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*Figure 1 – Sketch of the expander (meridional section)*

*Figure 2 – Share of rotor losses of the 5 kW expander*

*Figure 3 - Impeller 3D geometry*

*Figure 4 - Rotor computational grid (single sector, one blade passage and refined zones)*

*Figure 5 - Blade loading curves comparison for first-attempt and improved profiles*

*Figure 6 – Distributions of the angles for the two geometries*

*Figure 7 - impeller 3D improved geometry*

*Figure 8 – Distribution of relative velocity (Midspan layer, Improved geometry)*

*Figure 9 – Relative Mach Number distribution on meridional surface*



**Tables captions**

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*Table 1 – Main input data of the 5 kW expander*

*Table 2 – Main OD design results of the 5 kW expander*

*Table 3 - Physical properties of R134a working fluid*

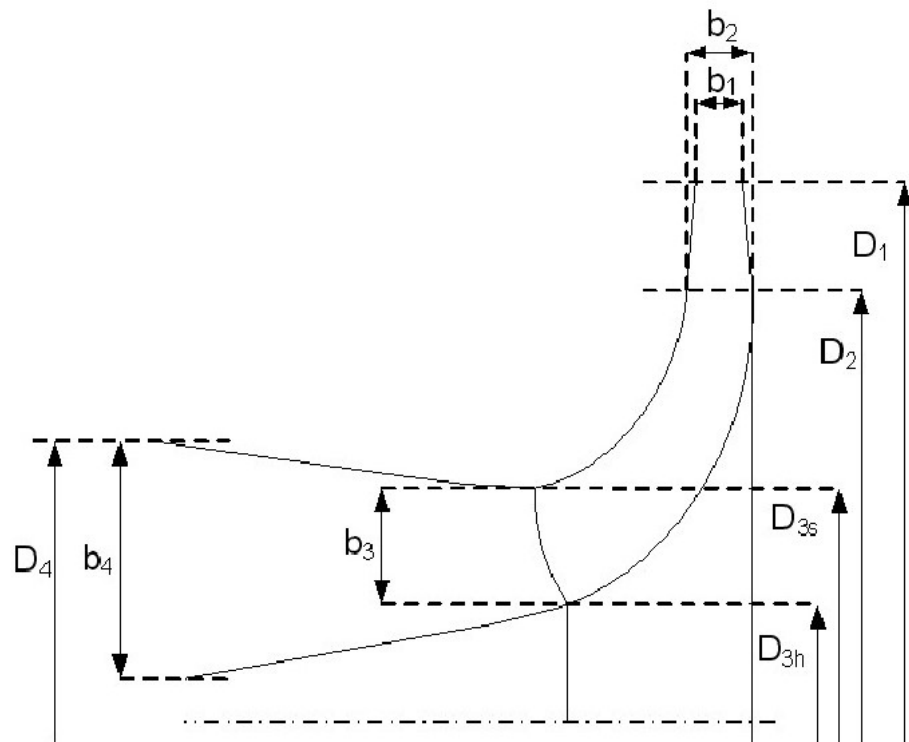
*Table 4 - CFD design main results - first attempt geometry*

*Table 5 - Comparison between OD design and 3D CFD design for initial geometry*

*Table 6 - CFD design main results - improved geometry*

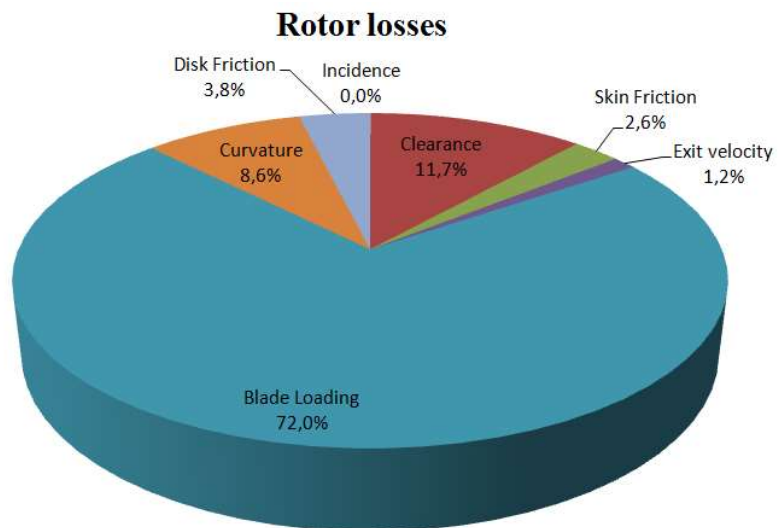
*Table 7 - Comparison between OD design and 3D CFD design for improved geometry*

474 **Figures**



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486 **Figure 1**



**Figure 2**

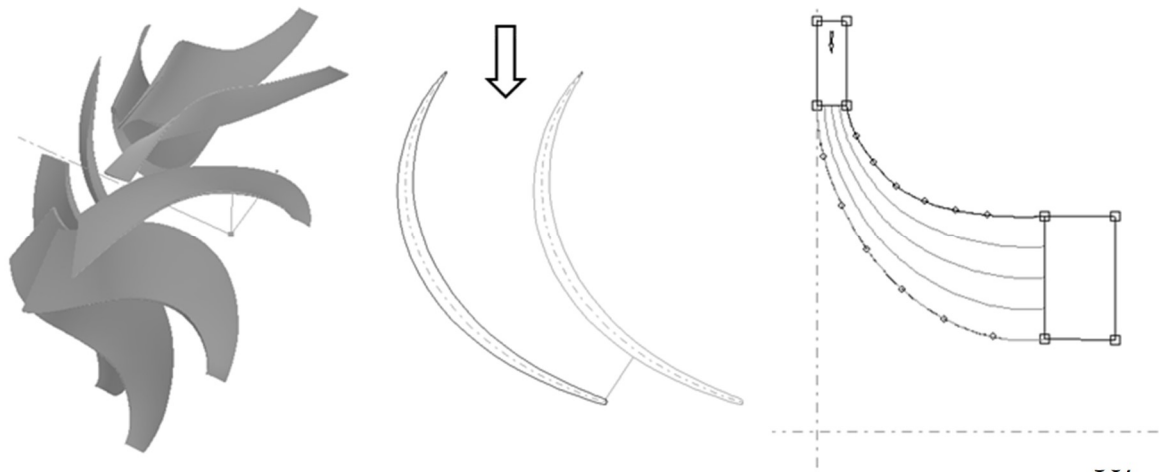


Figure 3

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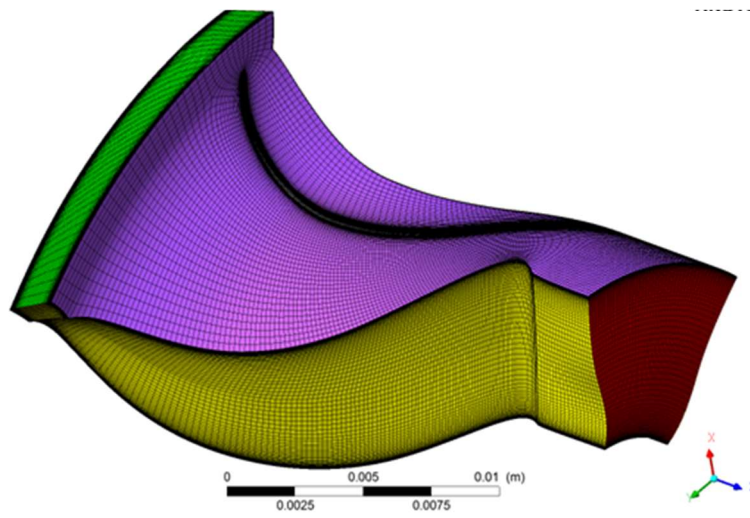
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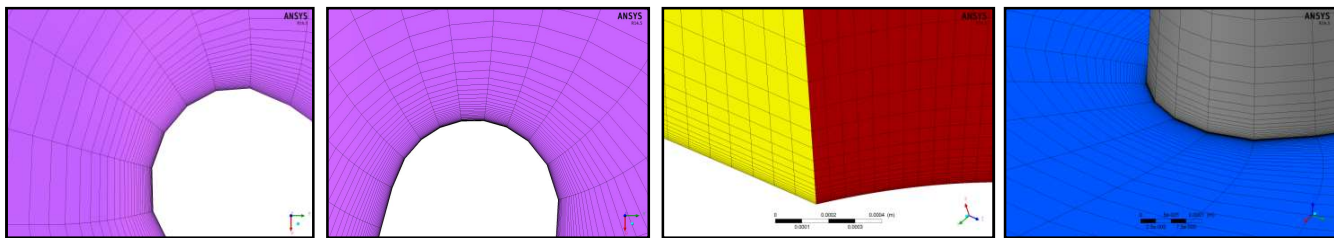


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LE - SHROUD

TE - SHROUD

PERIODIC/OUTLET

BLADE/HUB - LE

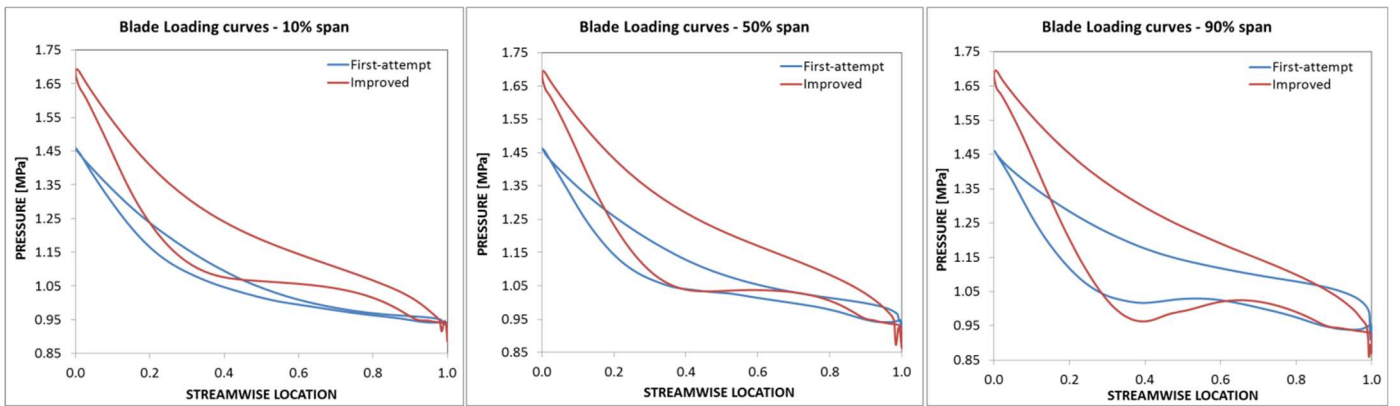
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Figure 4

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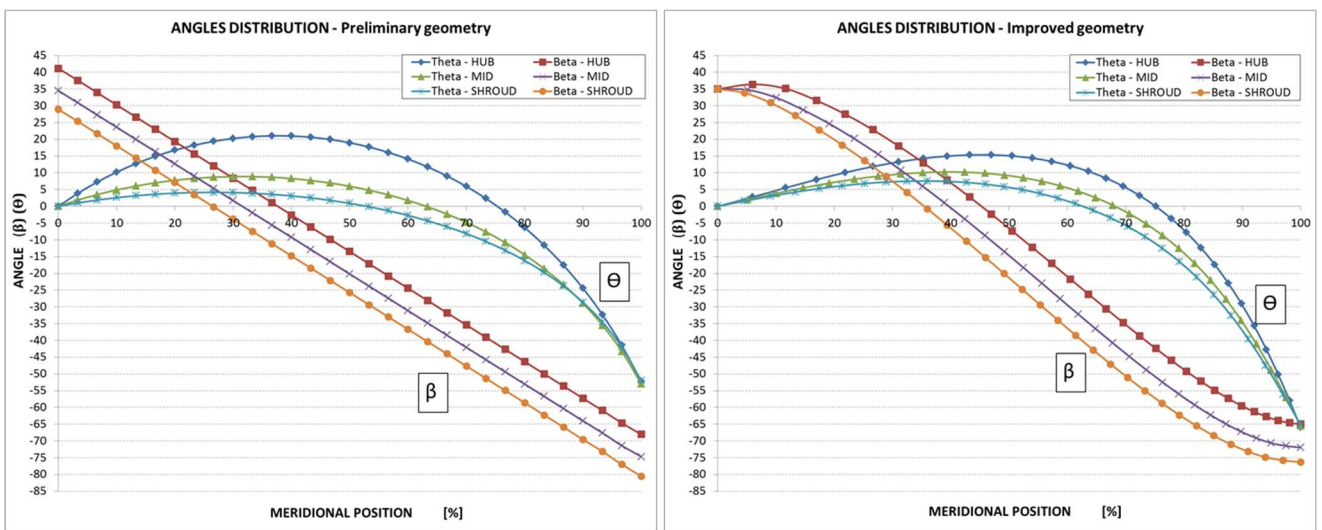
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Figure 5

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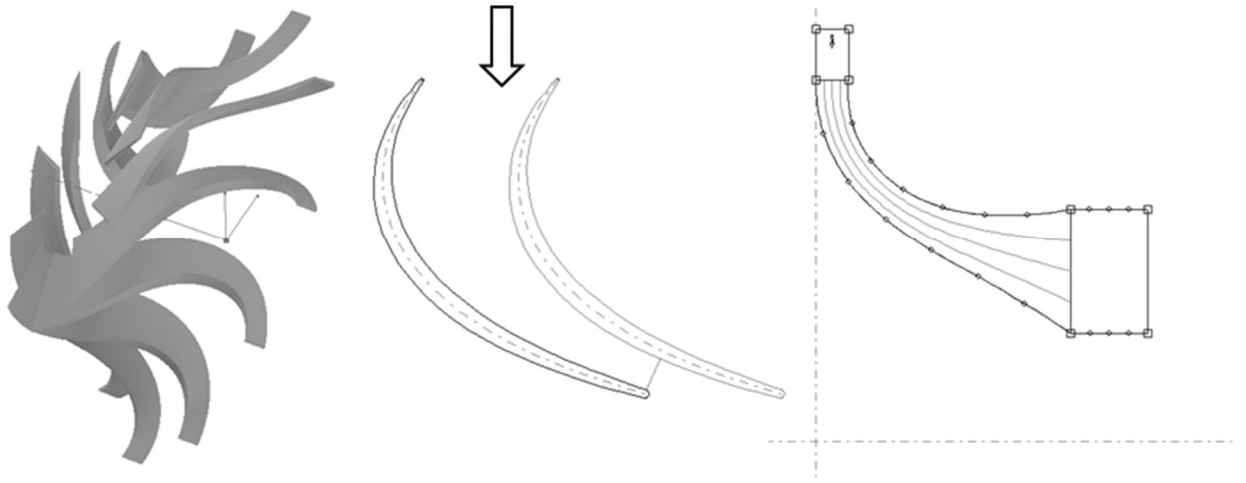
Figure 6

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Figure 7

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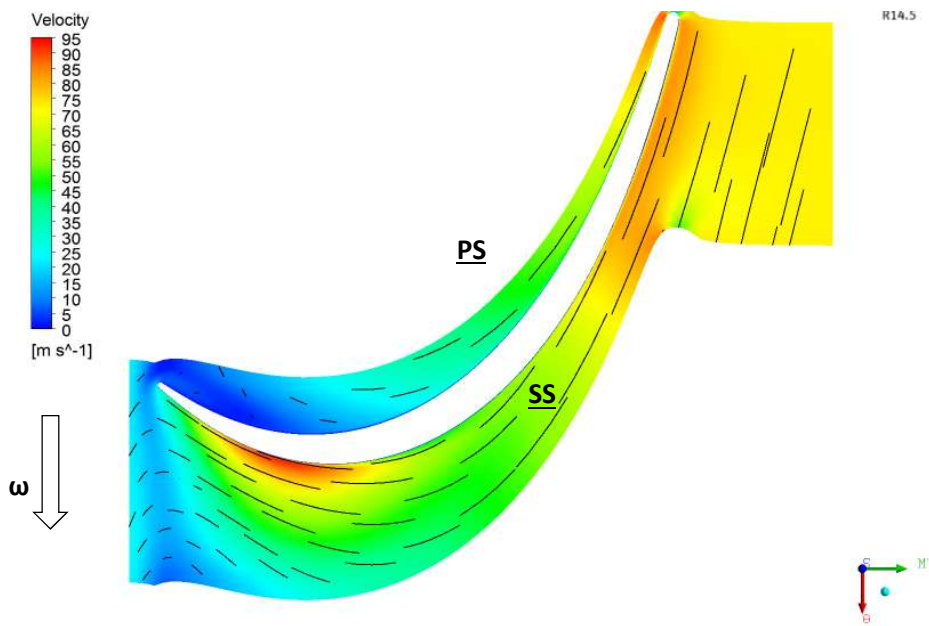
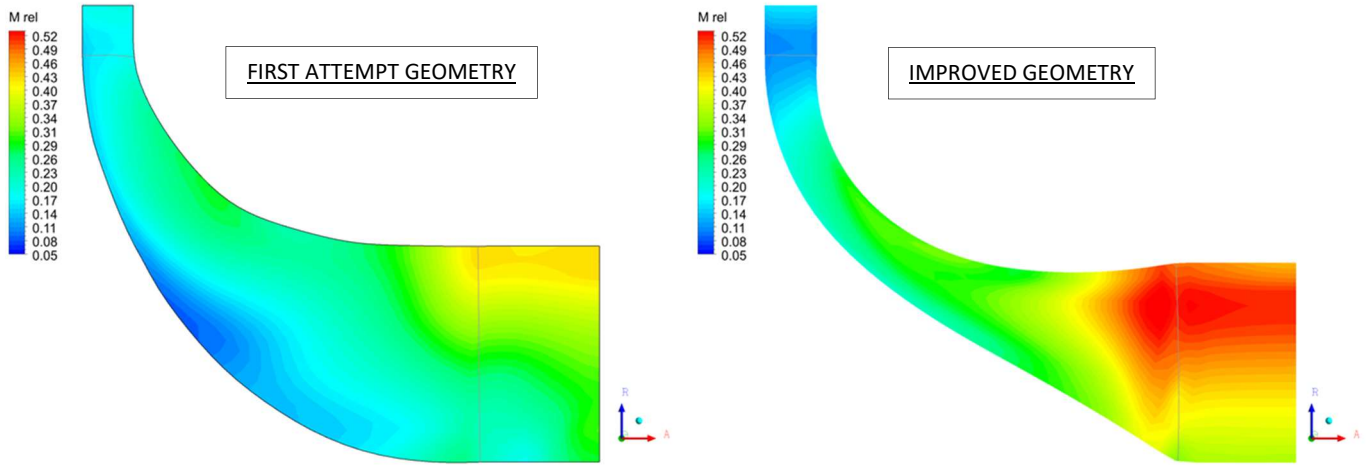


Figure 8

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Figure 9

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## Tables

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<b>Parameter</b>	<b>Value</b>	<b>Unit</b>
<i>Non-dimensional (Flow)</i>		
$\Psi$	0.995	[-]
$\Phi$	0.09	[-]
$R$	0.63	[-]
<i>Dimensional</i>		
$d_2$	0.035	[m]
$p_{01}$	3.8	[MPa]
$T_{01}$	420.15	[K]
<i>Non-dimensional (Geometry)</i>		
$d_1/d_2$	1.45	[-]
$d_3/d_2$	0.47	[-]
$d_4/d_3$	1.4	[-]
$L_D/D_3$	1.5	[-]
$b_2/d_2$	0.0452	[-]
$b_1/b_2$	1	[-]

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Table 1

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<b>Parameter</b>	<b>Value</b>	<b>unit</b>
<b>Power output (<math>P</math>)</b>	5093	[W]
<b>Mass Flow Rate (<math>\dot{m}</math>)</b>	0.1984	[kg/s]
<b>Angular velocity (<math>\Omega</math>)</b>	87,645	[rpm]
<b>Number of rotor blades <math>Z_B</math></b>	8	
<b>Isentropic enthalpy variation (<math>\Delta h_{stage}</math>)</b>	37,000	[J/kg]
<b>Absolute velocity inlet angle (<math>\alpha_2</math>)</b>	84.8	[°]
<b>Relative velocity inlet angle (<math>\beta_2</math>)</b>	-3.2	[°]
<b>Global rotor loss coefficient (<math>\xi_R</math>)</b>	3.409	[-]
<b>Total to Static efficiency (<math>\eta_{ts}</math>)</b>	0.6935	[-]
<b><math>c_2</math></b>	160.5	[m/s]
<b><math>c_3</math></b>	19.93	[m/s]
<b><math>w_2</math></b>	14.48	[m/s]
<b><math>w_3</math></b>	78.08	[m/s]
<b><math>u_2</math></b>	160.6	[m/s]
<b><math>u_3</math></b>	75.49	[m/s]
<b><math>V_{sound2}</math></b>	160.8	[m/s]
<b><math>V_{sound3}</math></b>	168.7	[m/s]
<b><math>Ma_{r2}</math></b>	0.090	[-]
<b><math>Ma_{r3}</math></b>	0.463	[-]
<b><math>p_{02}</math></b>	3.673	[MPa]
<b><math>p_2</math></b>	2.251	[MPa]
<b><math>p_{03}</math></b>	0.9409	[MPa]
<b><math>p_3</math></b>	0.9341	[MPa]
<b><math>\rho_2</math></b>	84.85	[kg/m <sup>3</sup> ]
<b><math>\rho_3</math></b>	33.97	[kg/m <sup>3</sup> ]
<b><math>T_2</math></b>	122.9	[°C]
<b><math>T_3</math></b>	97.53	[°C]

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Table 2

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<i>Physical property</i>	<i>Value</i>	<i>unit</i>
Specific Heat ( $c_p$ )	1,109	[J/kg-K]
Thermal Conductivity ( $k$ )	0.02065	[W/m-K]
Dynamic viscosity ( $\mu$ )	1.553e <sup>-5</sup>	[kg/s-m]
Molecular Weight ( $M_w$ )	102	[kg/kmol]
Reference Temperature ( $T_{ref}$ )	298.15	[K]
Critical Temperature ( $T_c$ )	374.2	[K]
Critical Pressure ( $p_c$ )	4.059	[MPa]
Critical Specific Volume ( $v_c$ )	0.001969	[m <sup>3</sup> /kg]
Acentric Factor ( $a_f$ )	0.3269	[-]

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Table 3

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<i>Variable</i>	<i>CFD</i>	<i>unit</i>
$\dot{m}$	0.1984	[kg/s]
$\eta_{ts}$	68.04	[%]
$P$	4,504	[W]
$p_2$	1.45	[MPa]
$p_{02}$	2.32	[MPa]
$p_3$	0.950	[MPa]
$p_{03}$	0.970	[MPa]
$T_{02}$	395.9	[K]
$T_{03}$	368.6	[K]
$h_{02}$	345,300	[J/kg]
$h_{03}$	322,600	[J/kg]

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Table 4

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<i>Variable</i>	<i>unit</i>	<i>OD design</i>	<i>3D CFD first attempt design</i>	<i>OD – 3D relative error [%]</i>
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$c_2$	[m/s]	160.5	158.3	-1.4
$c_3$	[m/s]	19.9	36.7	45.8
$\eta_{ts}$	[%]	69.90	68.04	-1.86
$P$	[W]	5,093	4,504	-11.6

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Table 5

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<b>Variable</b>	<b>CFD design</b>	<b>unit</b>
$\dot{m}$	0.2013	[kg/s]
$\eta_{ts}$	71.76	[%]
$P$	5,162	[W]
$Z_B$	10	
$p_2$	1.67	[MPa]
$p_{02}$	2.87	[MPa]
$p_3$	0.94	[MPa]
$p_{03}$	0.95	[MPa]
$T_{02}$	399.4	[K]
$T_{03}$	362.2	[K]
$h_{02}$	342,990	[J/kg]
$h_{03}$	317,348	[J/kg]

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Table 6

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<b>Variable</b>	<b>unit</b>	<b>OD Design</b>	<b>3D CFD Improved design</b>	<b>OD – 3D relative error [%]</b>
$c_2$	[m/s]	162.3	166.0	2.2
$c_3$	[m/s]	21.7	26.8	19.0
$\eta_{ts}$	[%]	72.78	71.76	-1.42
$P$	[W]	5,422	5,162	-4.8

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Table 7

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